



Document on reduction techniques for cement plants

TFTEI technical secretariat
Nadine Allemand (CITEPA)

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Agenda

- Objectives
- Limit values of the Gothenburg Protocol
- Reduction techniques and the costs
- Next steps

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Objectives of the work

- ✓ Update an existing document from 2005 and information developed for the revision of the Gothenburg Protocol

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Agenda

- Objectives
- Limit values of the Gothenburg Protocol and BAT AELs
- Reduction techniques and the costs
- Next steps

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Limit values in the Gothenburg protocol

Limit values for NO_x emissions released from cement clinker production^a

| <i>Plant type</i> | <i>ELV for NO_x (mg/m³)</i> |
|--|--|
| General (existing and new installations) | 500 |
| Existing lepol and long rotary kilns in which no waste is co-incinerated | 800 |

^a Installations for the production of cement clinker in rotary kilns with a capacity >500 Mg/day or in other furnaces with a capacity >50 Mg/day. The O₂ reference content is 10%.

Limit values for dust emissions released from cement production^a

| | <i>ELV for dust (mg/m³)</i> |
|--|--|
| Cement installations, kilns, mills and clinker coolers | 20 |

^a Installations for the production of cement clinker in rotary kilns with a capacity >500 Mg/day or in other furnaces with a capacity >50 Mg/day. The reference oxygen content is 10%.

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Reduction techniques for NO_x

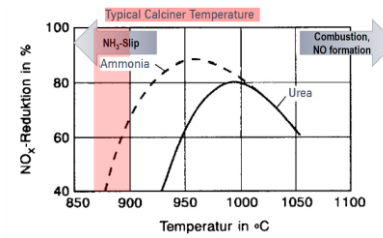
- ✓ Primary measures:
 - Flame cooling
 - Low NO_x burners
 - Staged combustion
 - Mild kiln firing
 - ...
- ✓ SNCR (Selective non catalytic reduction)
- ✓ SCR (Selective catalytic reduction)

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Reduction techniques for NOx

- ✓ Primary measures:
 - 500 mg/Nm³ at 10% O₂ daily average
 - Optimum condition frequently in conflict with the best setting for the kiln operation
- ✓ SNCR
 - Injection of an urea solution or an ammonia solution in the kiln calciner at around 900°C
 - An efficiency of 30 to 50% achieved with stoichiometry of 0.5 to 0.9 %
 - 60 to 80% achieved with stoichiometry (NH₃/NO_x) of 1.2 to 1.8 %
 - Able to reach 500 mg/Nm³, possible 200 mg/Nm³ in some specific cases
 - Ammonia split if optimal conditions not obtained

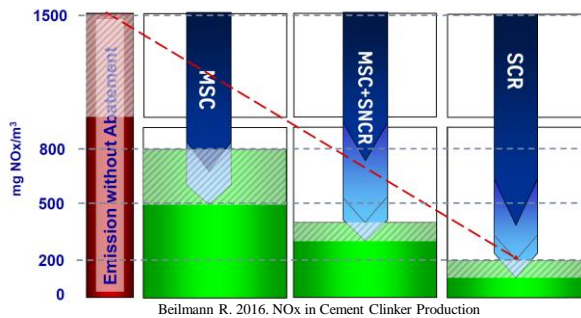


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Reduction techniques for NOx

- ✓ SCR
 - 200 mg/Nm³ at 10% O₂ daily average, can be obtained
 - 8 plants equipped in Europe in 2016



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BAT AELS for NO_x and NH₃

| Kiln type | Unit | BAT-AEL (daily average value) |
|-----------------------------|--------------------|---|
| Preheater kilns | mg/Nm ³ | < 200 – 450 ⁽¹⁾ ⁽²⁾ |
| Lepol and long rotary kilns | mg/Nm ³ | 400 – 800 ⁽³⁾ |

⁽¹⁾ The upper level of the BAT-AEL range is 500 mg/Nm³, if the initial NO_x level after primary techniques is > 1 000 mg/Nm³.

⁽²⁾ Existing kiln system design, fuel mix properties including waste and raw material burnability (e.g. special cement or white cement clinker) can influence the ability to be within the range. Levels below 350 mg/Nm³ are achieved at kilns with favourable conditions when using SNCR. In 2008, the lower value of 200 mg/Nm³ has been reported as a monthly average for three plants (easy burning mix used) using SNCR.

⁽³⁾ Depending on initial levels and NH₃ slip.

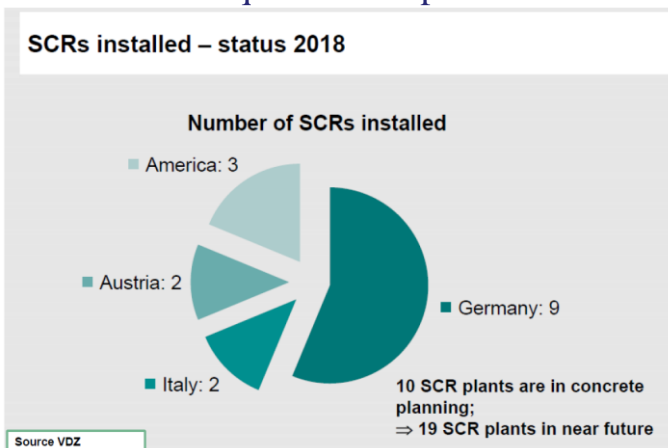
| Parameter | Unit | BAT-AEL (daily average value) |
|----------------------|--------------------|----------------------------------|
| NH ₃ slip | mg/Nm ³ | < 30 – 50 ⁽¹⁾ |

⁽¹⁾ The ammonia slip depends on the initial NO_x level and on the NO_x abatement efficiency. For Lepol and long rotary kilns, the level may be even higher.

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Equipment in NO_x emission reduction techniques in Europe



Source: Cinti J. Experience on NO_x emission reduction- TFTEI berlin workshop 2019

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Costs of SNCR for cement plants

| SNCR | | Updated cost data |
|---|--------------------|-------------------|
| Average daily NOx concentrations to be abated | mg/Nm3 at 10%O2 | 1200 |
| Outlet daily NOx concentrations reached | mg/Nm3 at 10%O2 | 800-400 |
| Investments (Capex) | kEuros | 1600 - 2000 |
| Operational cost (Opex) | Euro per t clinker | 0.3-1.0 |
| Electricity consumption | kWh per t clinker | 0.1-1.0 |

For a plant of 3000 t clinker per day :

- Emissions are reduced from 2650 t/year to 1770 or 880 t according to limit applied

Considering a lifetime of 20 y and 4% interest rate, the annual costs range between:

- 406 k€/y to 1110 €/year
- 0.42 to 1.15 €/t clinker
- 460 to 1250 €/t NOx abated

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Costs of SCR for cement plants

| SCR | | Updated cost data |
|---|--------------------|-------------------|
| Average daily NOx concentrations to be abated | mg/Nm3 at 10%O2 | 1200 |
| Outlet daily NOx concentrations reached | mg/Nm3 at 10%O2 | 200 |
| Investments (Capex) | kEuros | 5000-15000 |
| Operational cost (Opex) | Euro per t clinker | 0.3-1.1 |
| Electricity consumption | kWh per t clinker | 3-7 |

For a plant of 3000 t clinker per day :

- Emissions are reduced from 2650 t/year to 440 t

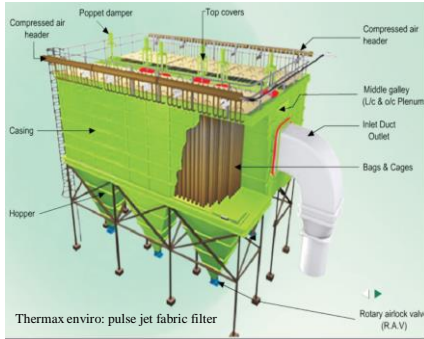
Considering a lifetime of 20 y and 4% interest rate, the annual costs range between:

- 655 k€/y to 2160 k€/year
- 0.70 to 2.15 €/t clinker
- 300 to 980 €/t NOx abated

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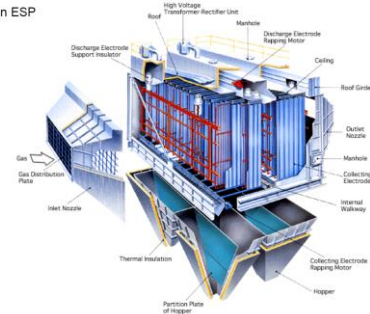
Reduction techniques for dust emissions



For the kiln firing processes and cooling and milling processes, BAT associated emission levels range from $<10 - 20 \text{ mg/Nm}^3$, as the daily average value. ESP and fabric filters are used

For diffuse emissions from dusty operations, reduction can be encapsulation of some operations, covering conveyors...

Inside an ESP



<https://www.indiamart.com/prodetail/retrofitting-of-electrostatic-precipitator-esp-6650529130.html>

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Costs of a fabric filter for cement plants

| Fabric filter | | Updated cost data |
|--|---|-------------------|
| Average daily PM concentrations to be abated | mg/Nm ³ at 10%O ₂ | 56 |
| Outlet daily PM concentrations reached | mg/Nm ³ at 10%O ₂ | 5 |
| Investments (Capex) | kEuros | 4000 - 10.000 |
| Operational cost (Opex) | Euro per t clinker | 0,3 |
| Electricity consumption | kWh per t clinker | 4,0 |

For a plant of 3000 t clinker per day :

- Emissions are reduced from 124 t/year to 11 t/year

Considering a lifetime of 20 y and 4% interest rate, the annual costs range between:

- 580 k€/y to 1020 k€/year
- 0.60 to 1.10 €/t clinker
- 5170 to 9100 €/t dust abated

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Reduction techniques for SO₂

SO₂ emissions from cement plants depend on the total input of sulphur compounds and the type of process used and are primarily determined by the content of the volatile sulphur in the raw materials and possibly by the fuels.

- ✓ Primary measures:
 - optimisation techniques, such as optimising the clinker burning process including the smoothing of kiln operation,
 - uniform distribution of the hot meal in the kiln riser
 - prevention of reducing conditions in the burning process
 - choice of raw materials and fuels
- ✓ Secondary measures when SO₂ emission are high
 - Addition of absorbent such as slaked lime, quick lime...to the raw material
 - Dry adsorption in a dry scrubber
 - Wet scrubber

The BAT AEL in daily average value ranges from < 50 to 400 mg/Nm³

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BAT AELs for SO₂

| Parameter | Unit | BAT-AEL ⁽¹⁾ ⁽²⁾ (daily average value) |
|--|--------------------|--|
| SO _x expressed as SO ₂ | mg/Nm ³ | < 50 – 400 |

⁽¹⁾ The range takes into account the sulphur content in the raw materials.

⁽²⁾ For white cement and special cement clinker production, the ability of clinker to retain fuel sulphur might be significantly lower leading to higher SO_x emissions.

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Costs of adsorbent injection for cement plants



| Adsorbent injection | | Updated cost data |
|--|--------------------|-------------------|
| Average dailySO2 concentrations to be abated | mg/Nm3 at 10%O2 | 600-1000 |
| Outlet daily SO2 concentrations reached | mg/Nm3 at 10%O2 | 400 |
| Investments (Capex) | kEuros | 200-750 |
| Operational cost (Opex) | Euro per t clinker | 0.3 - 0.7 |
| Electricity consumption | kWh per t clinker | 0.1 - 0.3 |

For a plant of 3000 t clinker per day :

- Emissions are reduced by 440 to 1320 t/y

Considering a lifetime of 20 y and 4% interest rate, the annual costs range between:

- 300 k€/y to 730 k€/year
- 0.30 to 0.80 €/t clinker
- 700 to 1650 €/t SO₂ abated

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Costs of wet FGD for cement plants



| Adsorbent injection | | Updated cost data |
|--|--------------------|-------------------|
| Average dailySO2 concentrations to be abated | mg/Nm3 at 10%O2 | 700 - 1300 |
| Outlet daily SO2 concentrations reached | mg/Nm3 at 10%O2 | 50 - 400 |
| Investments (Capex) | kEuros | 10.000-26.000 |
| Operational cost (Opex) | Euro per t clinker | 0.4-1.4 |
| Electricity consumption | kWh per t clinker | 8-10 |

For a plant of 3000 t clinker per day :

- Emissions are reduced by 660 to 2760 t/y

Considering a lifetime of 20 y and 4% interest rate, the annual costs range between:

- 1120 k€/y to 3260 k€/year
- 1.20 to 3.40 €/t clinker
- 1700 to 4900 €/t SO₂ abated

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Next steps

- Finalization of the second draft of document
- To be circulated in a small working group
- Finalization of the document by end of 2019

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Thank you very much
for your attention!
Questions?

TFTEI Technical Secretariat



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