



# Improvements of the TFTEI Cost Calculation Tool for Emission Reduction Measures in LCPs

TFTEI Technical Secretariat

25 June 2015

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## Agenda

- Current tool and methodology
  - Implementation of new developments
  - ✓ Improvement of user-friendliness
  - ✓ Part load operation
  - ✓ EPA-Method for NO<sub>x</sub>
  - Update of documentation
  - Improvement of database
  - Next steps
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### General cost methodology

|               |  |
|---------------|--|
| Fuels         | Coal, oil, gas, solid biomass (wood) in co-combustion with coal  |
| Fuel approach | Detailed and general approach  |
| Plants        | Boilers  |
| Pollutants    | NO <sub>x</sub> , SO <sub>2</sub> , PM   |
| Technologies  | NO <sub>x</sub> : LNB, SCR, SNCR<br>SO <sub>2</sub> : wet FGD, lime spray dryer, (dry process to be included)<br>PM: FF, ESP |

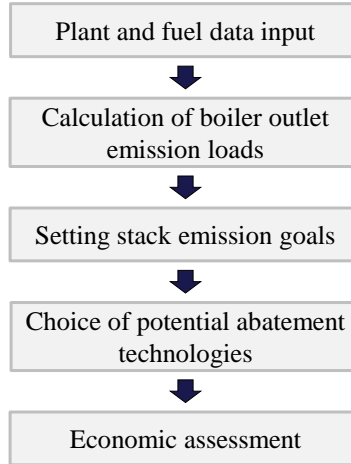
⇒ **Implemented in a VBA supported EXCEL-Tool**

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**Current tool and methodology**



### General cost methodology




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### Current tool and methodology



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Revision of the Front Page

|                                    | NO <sub>x</sub>  | SO <sub>2</sub>  | Dust  |
|------------------------------------|--|--|---|
| Natural Gas                        | <p>Natural Gas - NO<sub>x</sub></p> <p>incl. Primary Measures<br/>SCR<br/>SNCR</p> |  |   |
| Liquid Fuels                       | <p>Liquid - NO<sub>x</sub></p> <p>incl. Primary Measures<br/>SCR<br/>SNCR</p>      | <p>Liquid - SO<sub>2</sub></p> <p>incl. Fuel Substitution<br/>LSFO Flue Gas Desulfurization<br/>LSD Flue Gas Desulfurization<br/>DSI Flue Gas Desulfurization<br/>with Fabric Filter</p> | <p>Liquid - Dust</p> <p>incl. ESP</p>         |
| Solid Fuels<br>(coal and bio-mass) | <p>Solid - NO<sub>x</sub></p> <p>incl. Primary Measures<br/>SCR<br/>SNCR</p>       | <p>Solid - SO<sub>2</sub></p> <p>incl. Fuel Substitution<br/>LSFO Flue Gas Desulfurization<br/>LSD Flue Gas Desulfurization<br/>DSI Flue Gas Desulfurization<br/>with Fabric Filter</p>  | <p>Solid - Dust</p> <p>incl. ESP<br/>PJFF</p> |

**VBA Programming**



Parameter Check

Emission calculation has been modified in order to facilitate data collection for the user

⇒ Parameters that are only relevant for a specific pollutant have been taken out of consideration for other pollutants

⇒ Examples:

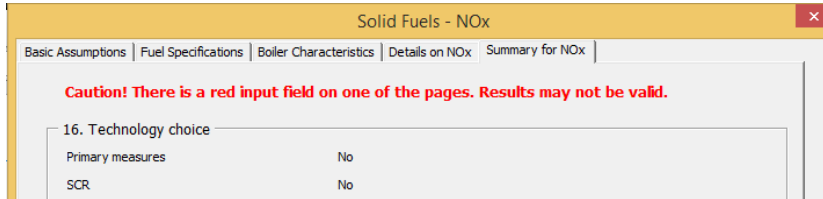
- Carbon in ash content
- Ash retained in boiler



**VBA Programming**



### Warning on Summary Page



- Instead of not showing the next VBA sheet unless all input fields are filled, they are now displayed from the beginning
- A red warning is shown on the summary page, if any input field is empty or outside the expected range
- This does not influence the appearance of the sheets for specific technologies, they still only appear if selected

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#### VBA Programming



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## VBA Implementation

- Part load operation is implemented as an option in the VBA sheet for every fuel and pollutant

4. Plant characteristics

Thermal power: 100 MW<sub>th</sub> [MWh]

Do you want to use part load operation?

5. Part Load Calculation

|                                | Full Load | Level 1 | Level 2 | Level 3 | Level 4 | Sum   |         |
|--------------------------------|-----------|---------|---------|---------|---------|-------|---------|
| Part load level                | 100       | 90      | 80      | 60      | 40      |       | %       |
| Operating hours per year       | 3000      | 500     | 1000    | 300     | 1500    | 6.300 | h       |
| NOx Boiler outlet emissions    | 400       | 380     | 350     | 300     | 280     |       | g/h     |
| Gross electric efficiency      | 38        | 37      | 36      | 34      | 33      |       | % (LHV) |
| Full load hours                | 3.000     | 462     |         | 201     | 691     | 5.199 | h       |
| Load dependent capacity factor |           |         |         |         |         |       | %       |
| Fuel consumption per year      |           |         |         |         |         |       | kg/h    |

Ref. Bo.:

### Part Load Operation



## Part Load Calculation

- Total operating hours and the load dependent capacity factor are calculated from the part load input.
- The following parameters are calculated for both, full load and annual average operation:
  - Fuel consumption
  - NO<sub>x</sub> emissions
  - Flue gas volume
- For design parameters, full load operation is taken into account, for consumption parameters (except electricity) annual average values (considering part load) are used.

### Part Load Operation



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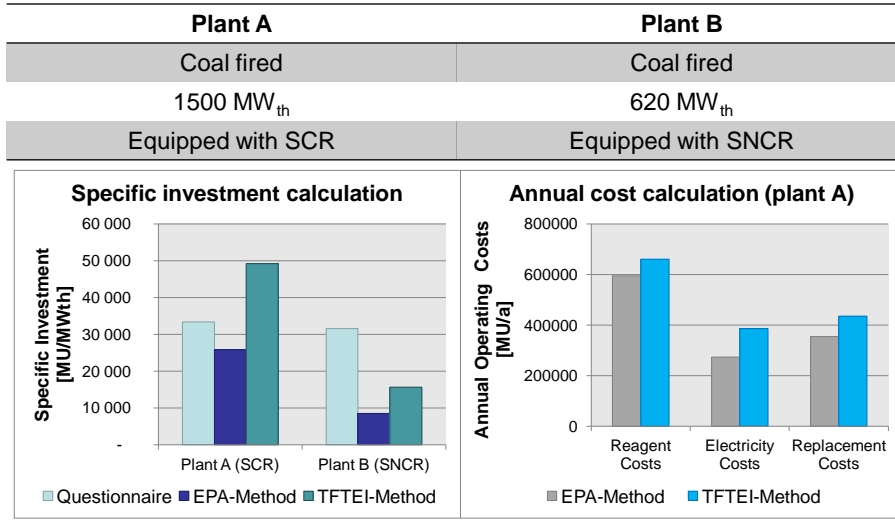
## Overview

- US EPA provided a methodology for emission reduction cost calculation (*Reference: Air Pollution Control Cost Manual, US EPA, 2002*)
  - The EPA method is implemented in the TFTEI tool for SO<sub>2</sub> and PM and shall also be used for NO<sub>x</sub>
  - The document addresses SCR and SNCR systems (no 1<sup>o</sup> measures) within these restrictions:
    - Only coal fired systems
    - SNCR with urea as reagent and from 0 to 50% NO<sub>x</sub> reduction
    - Minimum boiler size: 75 MW<sub>th</sub>
  - Methodology is more detailed and complex
    - More input data is necessary
    - Accuracy of results may be better (further testing is necessary)
    - Factors for cost calculation are up to 15 years old and hardly perspicuous
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### EPA Method for NO<sub>x</sub>



Quantitative Comparison



**EPA Method for NOx**



Qualitative Comparison

|                      | EPA  | TFTEI   |
|----------------------|--|---|
| <b>Advantages</b>    | Lower dependence on single parameters  | Literature based reference data   |
|                      | No experience with existing plants necessary (no assumption of specific investments)   | Higher transparency (no empirically determined factors), less complex calculations                |
|                      | More precise technical process reproduction in the economical equations  | Higher flexibility through specific investment adaptation   |
|                      | Documentation and calculation example available  | Less input parameters necessary   |
| <b>Disadvantages</b> | Many technical parameters necessary  | Strong dependence on specific investments   |
|                      | No individual influence parameter (e.g. specific investment) that takes the complexity/ circumstances of the system into account | Neglect of technical configuration (e.g. water consumption, tank size, size of the reactor, etc.) |
|                      | Few information on origin of cost factors  | Less detailed consideration of economic factors (contingencies, engineering, etc.)                |

**EPA Method for NOx**





## Implemented Aspects

- Only some minor contents of the EPA method have been implemented so far, as the results are not expected to become better if EPA is implemented with its current cost factors.
- Example: **Reagent dilution calculation**

| Reagent Solution                                      |         |
|---|---------|
| Concentration of reagent solution at delivery/storage | 29 %    |
| Concentration of reagent solution at injection        | 50 %    |
| Cost of water   | 2 €/t   |
| Cost of reagent at storage concentration              | 400 €/t |

- Main advantages:
  - ⇒ Reagent cost does not have to be converted to pure reagent (as it is usually bought as an aqueous solution).
  - ⇒ Cost of additional water can be calculated.

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### EPA Method for NO<sub>x</sub>



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### User Manual

- The user manual has been updated in order to suit the needs of the now implemented VBA programming.
- Due to the facilitations caused by the VBA programming, it is now shorter and less complicated.
- For expert users, a detailed documentation of the VBA programming is currently written to allow further improvements or trouble-shooting.



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**Documentation**



### Technical Document

- The new implementations have been introduced into the technical document
- This is especially relevant for
  - Part load operation
  - Reagent dilution calculation

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**Documentation**



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### Improvement of the database

- Goal:
    - Reducing the dependency of the cost methodology of the specific investment value.
    - Providing data for the TFTEI clearing house
  - EPA provides a methodology but the cost factors are outdated, so that the results might become worse if it is applied without modification.
  - TFTEI survey for NO<sub>x</sub> from 2012 is lacking of many technical parameters and the response was very low.
- ⇒ A new questionnaire is currently being developed to gather new/better data sets.
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### **Improvement of the database**



## LCP survey

- Anonymous web-based survey that is easy to use and adopts to the characteristics of the considered technology
- Target group:
  - Operators of LCP with NO<sub>x</sub> reduction technology implemented
- Contents:
  - More detailed technical parameters
  - Total investment
  - Annual operating costs
- Time schedule:
  - Distribution of the questionnaire within the following weeks

⇒ **Results can also be introduced into the TFTEI clearing house**

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**Improvement of the database**



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### Next Steps

- Sending out the questionnaire to members of TFTEI and other plant operators
  
- Promotion of the tool
  - Publication on new TFTEI web-site
  - Visit to IIASA
  - Workshop with EECCA countries



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Next Steps



Thank you very much  
for your attention!

TFTEI Technical Secretariat

