



# EGTEI Methodology

## Work to update costs for LCP

SO<sub>2</sub>, NO<sub>x</sub> and PM abatement techniques

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### **Aim of the work**

Update the methodology developed by EGTEI in 2005 in order to consider :

- combustion with thermal capacity > 50 MW
  - solid fuels, liquid fuels, gaseous fuels and biomass co-firing with coal
  - Fabric filter and ESP
  - Wet flue gas desulphurisation, semi-dry desulphurisation and dry desulphurisation
  - Consider primary measures for deNO<sub>x</sub>, SNCR and SCR
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## Organisation

- Work started by the end of 2011
  - Set up of a sub-group of experts (EDF, EON, CEFIC, ECN, Eurelectric, Concawe, EU turbines)
  - 6 EGTEI sub group meetings
  - Development of an EXCEL tool to estimate cost for a given plant consuming different fuels and of a document explaining of cost estimate developed
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## General Cost Methodology

Total annual cost	$C_{\text{tot}} \left[ \frac{\text{€}}{\text{year}} \right] = C_{\text{cap}} \left[ \frac{\text{€}}{\text{year}} \right] + C_{\text{op}} \left[ \frac{\text{€}}{\text{year}} \right]$
Annualisation of investment	$C_{\text{cap}} \left[ \frac{\text{€}}{\text{year}} \right] = C_{\text{inv}} \cdot \frac{(1+p)^n}{(1+p)^n - 1} \cdot p$
Composition of OPEX	$C_{\text{op}} \left[ \frac{\text{€}}{\text{year}} \right] = C_{\text{op,fix}} \left[ \frac{\text{€}}{\text{year}} \right] + C_{\text{op,var}} \left[ \frac{\text{€}}{\text{year}} \right]$
Fixed operating cost	$C_{\text{op,fix}} \left[ \frac{\text{€}}{\text{year}} \right] = C_{\text{inv}}[\text{€}] * f_{\text{O\&M}} \left[ \frac{\%}{\text{year}} \right]$
Variable operating cost	$C_{\text{op,var}} \left[ \frac{\text{€}}{\text{year}} \right] = \sum C^{\text{unit}} \left[ \frac{\text{€}}{\text{year}} \right]$

P = interest rate | n = equipment lifetime | unit = equipment, reagent and electricity consumption, disposal, etc.

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## General Cost Methodology

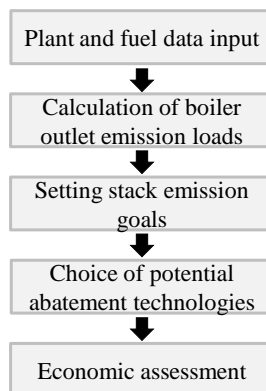
## Current Implementation

Fuels	Coal, oil, gas, solid biomass (wood)
Fuel approach	Detailed and general approach
Plants	Boilers
Pollutants	NO <sub>x</sub> , SO <sub>2</sub> , PM
Technologies	NO <sub>x</sub> : LNB, SCR, SNCR SO <sub>2</sub> : wet FGD, lime spray dryer, (dry process to be included) PM: FF, ESP

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### Calculation of boiler outlet emission loads

## Emission load calculation Approach

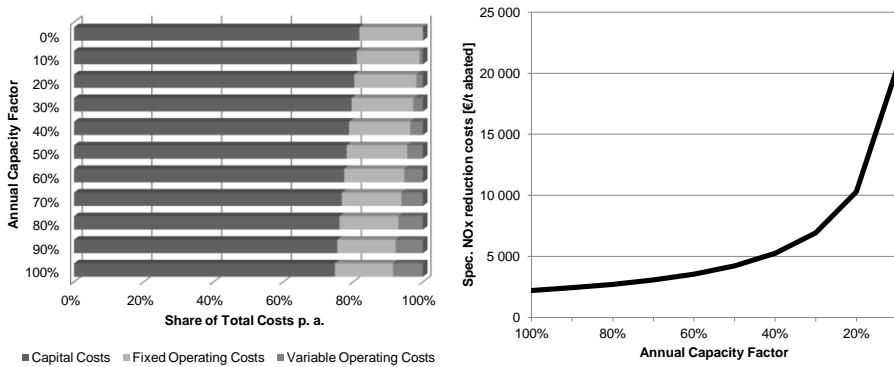


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### Calculation of boiler outlet emission loads

Example cost analysis  
- NO<sub>x</sub> abatement costs (SCR) -

Effect of **plant operation** (annual capacity factor) on cost composition (left) and spec. NO<sub>x</sub> reduction cost (right) of an SCR

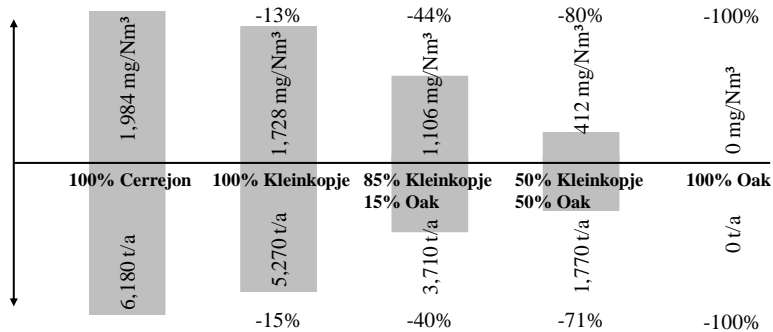


Calculation Basis: 1,000 MWth | 80 €/kWh SCR investment | 2% fixed O&M costs | 9% CRF | 80% reduction (400 to 120 mg/Nm<sup>3</sup>)

**Economic assessment of DeNOx technologies**

Calculation of boiler outlet emissions  
- exemplary case for SO<sub>2</sub> -

Fuel	C	H	O	N	S	Ash	Moisture
Cerrejon (CO)	83.40	4.95	9.47	1.37	0.81	8.41	11.83
Kleinkopje (RSA)	85.02	4.74	7.33	2.19	0.72	14.49	7.71
Oak	50.64	6.23	41.85	1.28	0.00	10	40



Calculation Basis: 500 MW<sub>th</sub> | Operating hours: 6,000

**Economic assessment of DeNOx technologies**



### Next steps

Work delivered to UNECE / WGSR (next meeting end of June 2014)  
Work to be delivered before mid may at the latest.

Work also delivered to IPTS Seville in the scope of the revision of the LCP BREF by the end of the year.

In between, circulation of the documents and the EXCEL file for comments

Comments expected by the end of November

Organisation of a meeting with CEFIC to test the methodology for different cases, especially for plant between 50 and 300 MWth

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**Thanks to the EGTEI technical secretariat and experts from the  
LCP working group**

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